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Performance of a Solar Chimney for Cooling Building Façades under Different Heat Source Distributions in the Air Channel

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Abstract— Solar chimneys can be employed in buildings for natural ventilation, cooling, or heating of the building envelope, hence saving energy. In open double-skin facades, the air channel's thermal effects between the two layers of a façade are similar to those in a solar chimney. Most studies about solar chimney in the literature have been focusing on heating one air channel wall. In this study, the performance of a solar chimney under different distributions of the heat source on both walls of the air channel was studied numerically by the Computational Fluid Dynamics method. Induced flow rate, temperature rise, and thermal efficiency of the chimney were investigated. Chimneys with practical dimensions with the height ranging from 0.5 m to 1.5 m and the gap—to—height ratio ranging from 0.025 to 0.15 were examined. The results showed that together with the chimney. While heating the whole left wall induced more flowrate than heating the whole right wall, heating part of the left and the right walls resulted in peak performance at specific portions of the right wall heated from the bottom or the top of the channel. The peak values of the investigated parameters and the specific portions of the heated wall to achieve those peaks also changed with the channel's gap—to—height ratio.

Keywords- Solar chimney; natural ventilation; building façade; heat source; CFD

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I. INTRODUCTION

Among the methods for controlling solar heat gain of buildings to save energy, double – skin façade (DSF) has been proved to be effective [1]–[3]. Quahtan [3], studying the thermal performance of a double–skin façade of a building in Malaysia, reported that the maximum temperature difference of indoor-outdoor temperature was up to 6°C for a un–airconditioned space. In Qatar, a DSF covering 40% of the walls could reduce 11.3% of the building's total heat gain [2].

The air cavity inside a DSF can be closed or opened [1], [4]. When the cavity is opened, absorbed solar radiation heats the air in the cavity and induces thermal or stack effect, a wellknown phenomenon in solar chimneys [5]. Therefore, results from solar chimneys studies can be applied to DSFs with similar configurations [4].

Several studies about solar chimneys have been reported, as summarized by Saadatian et al. [6] and Shi et al. [7]. Most of them focused on examining factors influencing solar chimneys' performance [8]–[17]. The factors have been reported in two major groups: structural and environmental

[7]. The structural group's main parameters were the chimney's dimensions, including the width of the cavity, the air gap, and the air channel's height. Solar radiation seemed to be the most critical environmental factor. Also, previous studies [17], [18] also reported that the distribution of the heat source inside the air channel also affected the performance of solar chimneys. Their results showed that heating one side or both sides of the air channel could significantly change the induced airflow rate. However, in previous research, the heat source was distributed on a whole wall of the channel. Cases where the heat source distributes on a portion of the channel's walls, have not yet been reported.

In this study, a solar chimney's performance with the heat source distributing on a portion of each air channel wall was studied numerically. The performance was assessed through three main parameters: the induced flow rate, the temperature rises through the air channel, and the thermal efficiency of the chimney.

II. MATERIAL AND METHOD

A. Problem Description

The studied problem is sketched in Figure 1. A building is assumed to have a two-layer wall; the inner layer can be a concrete wall, while the outer one can be a glazed or opaque plate. In the case of a glazed wall, solar radiation is transmitted through the glazing and absorbed by the inner wall. For the other case, the outer wall is an opaque plate such as a metal sheet. It is heated by solar radiation. In either case, the absorbed heat is transferred to the air inside the gap through natural convection. If the façade has open ends, an airflow is induced due to the warmed air's thermal effects. The airflow may help to reduce the solar heat gain, hence cooling the façade.

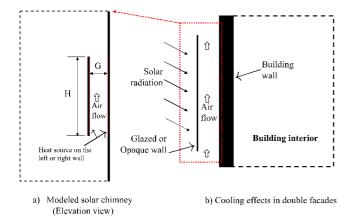


Fig. 1 Schematic of natural convection flow in a double façade and according to the modeled solar chimney

It is assumed that the dimension of the façade, which is normal to the plane in Figure 1, is larger than the gap of the cavity between the two layers of the wall. Consequently, the cavity can be modeled as a two-dimensional solar chimney [18], shown in Figure 1. The channel gap and height are denoted as G and H, respectively. The chimney is attached to a vertical wall that models the inner wall of the building. Heat source on either side of the wall is described by applying uniform heat flux on the inner surface of the air channel of the chimney. In the case of a glazed outer wall, the heat flux is assigned on the air channel's right wall in Figure 1. However, for an opaque outer wall, the heat flux should be assigned on the air channel's left wall. For intermediate cases where part of the outer wall is glazed while the remaining is opaque, the modelled heat source should be applied according to portions of both the left and the right wall of the air channel, as described in Figure 2.

B. Governing Equations

The governing equations for the airflow and heat transport in the solar chimney include conservations of continuity, momentum, and energy. The airflow and heat transfer were assumed to be steady. The flow was incompressible. Using the two-dimensional Reynolds Averaged Navier – Stokes (RANS) equations, the governing equations are as follows [18,19,20]:

$$\frac{\partial U_j}{\partial x_j} = 0 \tag{1}$$

$$\frac{\partial (U_i U_j)}{\partial x_j} = -\frac{1}{\rho} \frac{\partial P}{\partial x_i} - g_i \beta (T - T_{ref}) + \frac{\partial}{\partial x_j} \left(\nu \frac{\partial U_i}{\partial x_j} - \overline{u_i u_j} \right) (2)$$

$$\frac{\partial (TU_j)}{\partial x_j} = \frac{\partial}{\partial x_j} \left(\frac{\nu}{\Pr \frac{\partial T}{\partial x_j} \overline{T'u_j}} \right)$$
(3)

Where i and j indices denoting the horizontal and vertical directions; U, u and T, T are respectively time-averaged and fluctuating velocities, and time-averaged and fluctuating temperatures; T_{ref} is the reference temperature taken as the ambient one; P is the pressure; ρ and v are the air density and kinematic viscosity; β is the air thermal expansion coefficient; Pr is the Prantl number, indicates a time-averaged quantity. In equation (2), the Boussinesq approximation was applied for the variation of the air density with temperature, as suggested in previous studies [18], [20], [21].

For the turbulent stress $\overline{u_i u_j}$ and turbulent heat flux $T'u_j$, typical RANS turbulence models such as standard $k - \omega$, $k - \omega$ with modifications for low-Reynolds-number effects (low-Re $k - \omega$), $k - \varepsilon$, and RNG $k - \varepsilon$ [22] can perform well for this problem [18,20].

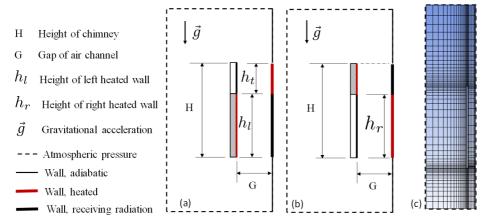


Fig. 2 Computational domain and boundary conditions for two cases of heating location: (a) on the left wall and (b) on the right wall; and (c) mesh structure

In this study, four models were applied to predict the induced flow rate through a solar chimney in the experiment by Yilmaz and Fraser [23], the low-Re $k-\omega$ offered the best

convergence rate and the best agreement between the computed flow rate and the measurements, as seen in Figure 3. Therefore, it was selected.

The governing equations, Equation (1)–(3) was discretized on a structured mesh, as shown in Figure 2c, using Finite Volume Method with the ANSYS Fluent CFD code (Academic version 2019R3). For the coupling between the continuity equation and the momentum equation, the SIMPLEC method [19] was employed.

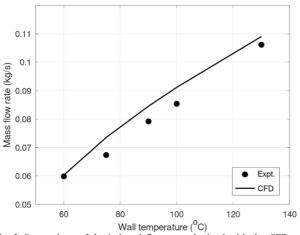


Fig. 3 Comparison of the induced flow rate obtained with the CFD model versus the experimental values by Yilmaz and Fraser [23]

C. Computational Domain and Boundary Conditions

The computational domain is described in Figure 2a and 2b. It covered both the air channel and the ambient air. The extension of the air channel's domain is necessary to allow the airflow to adapt to local flow conditions at the inlet and outlet of the air channel [18]. Following the suggestions by Gan [18], the extensions of the domain in Figure 2 were $10.0 \times G$ above, $5.0 \times G$ below, and $5.0 \times G$ to the left of the air channel. Larger domains were also tested. It was seen that the induced flow rate changed less than 0.5% as the domain was further enlarged.

As the right side of the domain in Figure 2a and 2b coincided with the building wall (Figure 1a), it was modeled as a non-slip wall. Other boundaries of the domain were assigned with atmospheric pressure, as they were open. For simplicity, heat conduction through the outer wall of the chimney was not modeled. The surfaces of the outer wall were applied with no-slip conditions. Inside the air channel, only the left and the right walls participated in the heat transfer. Generally, part of the outer wall may be either glazed or opaque, while the remaining had the opposite optical property. Assumed that the lower portion of the left wall, whose length is h_l , was opaque, uniform heat flux condition was applied on h_l . As the upper part of the left wall was glazed, the solar radiation should be absorbed by the upper part of the right wall over a length of $h_t = H - h_l$. Accordingly, uniform heat flux condition was applied on the portion h_t of the right wall. Similarly, h_r denotes the right wall's length with uniform heat flux for a glazed portion of h_r of the left wall. The remaining upper part of the left wall $(H - h_r)$ was assigned with heat flux.

Radiative heat transfer between the left and the right walls of the air channel was allowed in the model. The process was calculated by the S2S model in the ANSYS Fluent software [24]. A non-uniform structured rectangular mesh was used as presented in Fig. 2c. The mesh was clustered near the solid boundaries, particularly the air channel's heated walls, and higher mesh densities were also distributed at the inlet and outlet of the air channel.

To check the mesh-independence, the CFD model was run with the solar chimney tested by Yilmaz and Fraser [23] with H=3.0 m and G=0.1 m and a heat flux of 360.3 W/m². Different mesh resolutions were employed to obtain the induced mass flow rate through the channel. It was observed that, as the number of mesh elements increased, the flow rate changed below 1.0% when the maximum non-dimensional distance of the first grid point from the solid boundaries, or y⁺, was less than 2.0. This number was equivalent to 150 and 200 cells in the G and H directions inside the air channel. This required value of y⁺ was close to the findings by Zamora and Kaiser [20], which was below 1.0.

D. Validation

The CFD model was validated against the measurements by Yilmaz and Fraser [23]. In their experiments, the induced flow rate was measured through a solar chimney with H=3.0 m, G=0.1 m, and the third dimension of 1.0 m. Various heat fluxes were applied on one side of the air channel, and according to wall temperatures were from 60°C to 130°C. The measured and computed induced flow rates were plotted together in Figure 3, as functions of the wall temperature. The maximum discrepancy between the two results was 9.2%. Therefore, the model can reproduce well the measured data.

III. RESULTS AND DISCUSSIONS

The validated CFD model was employed to predict the induced flow rate, temperature rise through the chimney described in Figure 1a, and its thermal efficiency. These parameters were examined as the following factors changed: Location of the heat source, i.e., on the left or the right wall; length of the heat source: h_r and h_l ; chimney height H=0.5 m, 1.0 m, and 1.5 m; and the gap–to–height ratio G/H=0.025, 0.05, 0.075, 0.1 and 0.15. The applied heat flux was kept to 600 W/m² in all tests.

A. Flow Rate

The induced flow rate through the solar chimneys with different heights and gap-to-height ratios is presented in Figure 4 as the functions of the normalized length of the heated portion of the right wall, h_r/H or h_t/H . As h_r and h_t denote the heated portions of the air channel's right wall from the bottom and the top, respectively, $h_r/H = 0$ or $h_t/H = 0$ indicates that the whole left wall is heated. In contrast, for $h_r/H = 1.0$ or $h_t/H = 1.0$, the whole right wall is heated. For intermediate values of h_r/H or h_t/H , both walls are heated at according to portions as sketched in Figure 2a and 2b.

The results in Figure 4 show that the induced flow rate increased with the gap, for a given chimney height H, and either case of heating. The flow rate also increased with the chimney height. These trends have also been reported in the literature [17], [18], [21], [25].

At the gap-to-height ratio (G/H) of 0.025, the flow rates obtained with h_r and h_t were indistinguishable from each other. However, as G/H increased, the difference became more visible. In both heating cases, the flow rate increased with hr and ht, achieved a peak, and then decreased. Although the difference between the two maximum flow rates was minor, the peaks' positions were different. The peaks were at $h_r/H \approx$ 0.2 and $h_t/H \approx 0.7$, for heating the right wall from the bottom and the top, respectively. The two flow rates matched at $h_{r}/H = h_t/H \approx [0.35 - 0.4]$.

For the cases of heating the whole left wall $(h_{t'}/H = h_{t'}/H = 0)$ or the whole right wall $(h_{t'}/H = h_{t'}/H = 1.0)$, the results in Figure 4 show that heating the whole left wall induced more flow rate. The difference was more significant as the G/H ratio increased. Nguyen and Wells [17] reported similar results in studying the induced flow rate through a solar chimney attached to a vertical wall. However, this trend is different from the results for a stand-alone vertical solar chimney [18]. Gan [18] showed that heating one side of the channel induced less flowrate than when both sides of the channel were heated with the same total heat flux.

The flow fields together with the temperature distributions for the chimney with H=0.5 m, G/H=0.025 and 0.15, $h_r/H = h_t/H = 0.8$ are shown in Figure 5. For G/H=0.025, the temperature and velocity fields were similar for both cases of heating. The thermal boundary layer expanded from the heated surfaces and occupied the whole channel gap at the outlet. Accordingly, the induced flow rates were identical, about 0.053 kg/s, as seen in Figure 4a. For G/H=0.15, the thermal boundary layer near the right wall was thicker for $h_r/H = 0.8$, while that near the left wall had a higher temperature. The temperature rise at the air channel outlet was 10.3 K and 9.0 K for $h_r/H = 0.8$ (Figure 5c) and $h_t/H = 0.8$ (Figure 5d), respectively. As a result, the induced flow rate for $h_r/H = 0.8$ was higher, as seen in Figure 4.

B. Temperature Rise through the Chimney

As the air in the channel receives heat from the walls, its temperature rises. The temperature rise is defined as follows:

$$\Delta T = T_o - T_i \tag{4}$$

Ti and To are the air temperature at the inlet (bottom) and the air channel's outlet (top).

The temperature rise through the examined chimneys is plotted in Figure 6. For each H, the highest temperature rise was seen at the lowest gap-to-height ratio, G/H=0.025. At all heights, ΔT decreased as G/H increased. This observation is opposite to that of the flow rate in Figure 4.

It is seen that at large G/H ratios (G/H=0.15 and 0.1), heating the right wall from the top (h_t) yielded a higher temperature rise. As G/H became smaller, heating the right wall from the bottom (h_r) tended to produce higher ΔT at the lower range of $h_{t'}/H$ or $h_{t'}/H$. The point where the same ΔT values obtained with both heating cases gradually moved to the right ($h_{t'}/H$ or $h_{t'}/H \rightarrow 1.0$). Until H=0.5 m and G/H=0.025, heating from the bottom (hr) resulted in an entirely higher temperature rise.

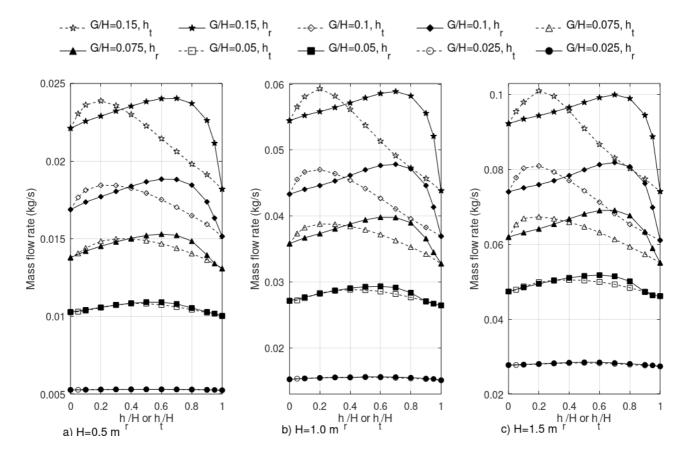


Fig. 4 Induced mass flow rate through the chimneys

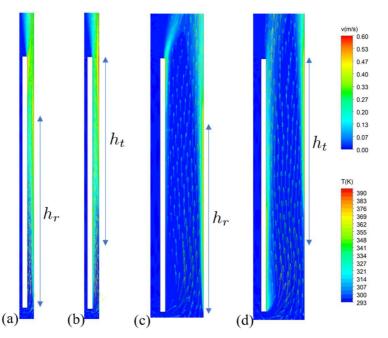


Fig. 5 Flow and temperature fields for H=0.5 m: (a) G/H=0.025, $h_r/H=0.8$; (b) G/H=0.025, $h_r/H=0.8$; (c) G/H=0.15, $h_r/H=0.8$; and (d) G/H=0.15, $h_r/H=0.8$; $h_$

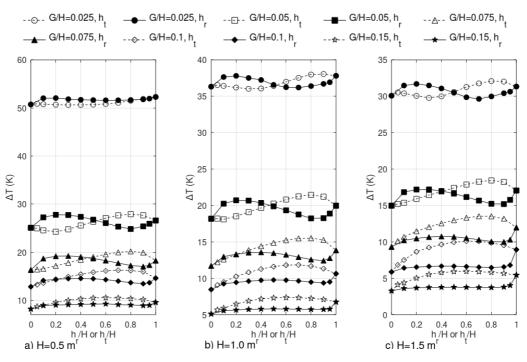


Fig. 6 Temperature rise through the chimneys

C. Thermal Efficiency

Thermal efficiency has been used to evaluate the performance of solar chimneys [17,25]. It is defined as the ratio between the heat gain of the airflow through the air channel Q_o and the heat supplied in the air channel Q_i :

$$\eta = Qo /Qi = \dot{m}cp \Delta T / Qi$$
 (5)

where \dot{m} is the induced mass flow rate, and c_p is the specific heat capacity of air.

Figure 7 presents the thermal efficiency η of the tested chimneys. In general, η changed significantly with h_r/H and

 h_t/H , except for G/H=0.025 where it was almost constant and varied slightly about 0.95.

At a given H, η decreased with the increase of G/H. From Figure 4, \dot{m} increased with G/H. However, in Figure 6, ΔT decreased with G/H. For example, for H=0.5 m, changing G/H from 0.05 to 0.1 increased the average flow rate from 0.013 kg/s to 0.017 kg/s (Figure 4) but reduced the temperature rise from about 26 K to about 14.5 K (Figure 6). Therefore, the decreasing rate of ΔT was more than the increasing rate of \dot{m} and equation (5) resulted in a decrease of η with G/H.

At a given G/H, increasing the chimney height offered lower thermal efficiency. This trend is seen in both cases of

heating. Comparing η of heating from the bottom, h_r , to heating from the top, h_t , the latter had higher thermal efficiency at higher G/H ratios. As the G/H ratio decreased, the difference of η between the two heating cases was negligible. This result is consistent with the trends of the data in Figure 4 and 6.

Heating the whole right wall $(h_r/H = h_t/H = 1.0)$ offered slightly higher thermal efficiency than heating the whole left wall $(h_r/H = h_t/H = 0)$. The peaks of the thermal efficiency in Figure 7 also changed with the G/H ratio. As G/H increased, the peak moved toward higher h_r/H but to smaller h_t/H . Particularly, at G/H=0.05, the peak thermal efficiencies were close to 1.0 at $h_r/H \approx 0.3$ and $h_t/H \approx 0.7$.

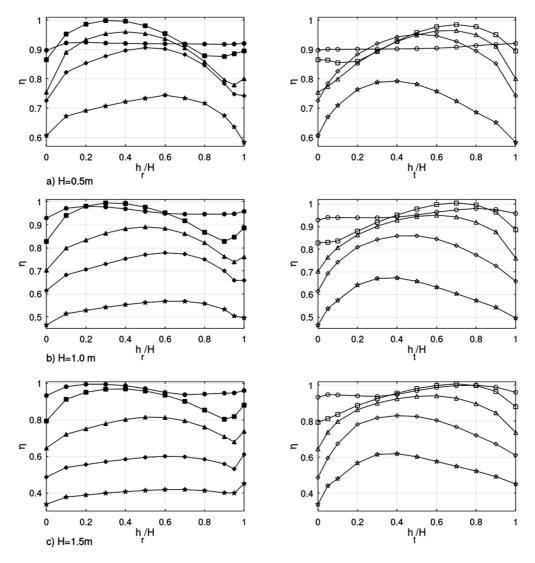


Fig. 7 Thermal efficiency of the solar chimneys

IV. CONCLUSION

The results show that, together with the solar chimney dimensions, the heat source's location and distribution in the air channel also strongly affected its performance. When the heat source was distributed on a whole wall of the air channel, heating the left wall (Figure 1a) induced more flow rate. Heating part of the right and the left walls resulted in identical flow rates at the low gap-to-height ratio. As the gap-to-height ratio increased, heating the lower part of the right wall achieved the highest flowrate at $h_r/H \approx 0.7$. The peak flow rate for heating the upper part of the right wall was at $h_t/H \approx 0.2$. Two heating cases resulted in the same flow rate at $h_r/H = h_t/H \approx [0.35 - 0.4]$.

While the induced flow rate increased with the gap-to-height ratio, the temperature rises through the chimney and the thermal efficiency decreased. As the gap-to-height ratio increased, heating the upper part of the right wall offered higher temperature rise and thermal efficiency. With a higher gap-to-height ratio, the thermal efficiency peak values moved toward higher h_{r}/H but smaller h_{t}/H . Significantly, the highest thermal efficiencies were close to 1.0 at the gap-to-height ratio of 0.05 and $h_{r}/H \approx 0.3$ or $h_{t}/H \approx 0.7$.

As this study was conducted in two dimensions, for future works, three – dimensional simulations or experiments can be conducted to investigate effects of the sidewalls, particularly with different heat source distributions on the sidewalls, on the performance of the chimney.

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